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### PRODUCTION OF Mg–Li ALLOYS BY ALUMINOTHERMIC VACUUM REDUCTION

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### Abstract

Mg-Li alloys are the lightest metallic construction materials and one of the most representative light alloys. The process of producing Mg-Li alloys by vacuum aluminothermic reduction, using magnesite and lithium carbonate as raw materials, was studied. The influence of reduction parameters on the extents of reduction of MgO and  $Li_2O$  was investigated. The results show that Mg-Li alloys can be produced by vacuum aluminothermic reduction using calcined magnesite and lithium carbonate. MgO was relatively easier to reduce by aluminum than  $Li_2O$ . Almost all MgO was reduced to Mg and more than 96% of  $Li_2O$  was reduced to Li. The main phase in the reduction slag was  $Li_2O$ •5 $Al_2O_3$ . The reaction mechanism was discussed. Vacuum aluminothermic reduction can be considered as a highly efficient and environmental friendly method for producing Mg-Li alloys.

Keywords: Mg-Li alloy; Vacuum aluminothermic reduction; Magnesite; Lithium carbonate; Li,0•5Al,0,

### **1. Introduction**

Magnesium–lithium alloys are the lightest metallic construction materials, having a specific gravity of 1.30–1.65 g/cm<sup>3</sup>, which is about 50% lighter than aluminum alloys and 10%–30% lighter than common magnesium alloys. They are therefore known as superlight alloys [1-3]. Because of their specific strength, rigidity, and good damping capacity, Mg–Li alloys have been widely explored in applications in the aircraft, electronics, and communication industries [4, 5].

There are three main methods of producing Mg–Li alloys: mixing molten magnesium and lithium, electrochemical reduction and vacuum thermal reduction. Because Mg and Li are very active elements, their metals are prone to oxidize and burn during melting in air. Mg–Li alloys produced by mixing metallic magnesium and lithium are always conducted in a frequency induction furnace protected by argon, which demands strict operating procedures and leads to high production costs [6]. Preparation of Mg–Li alloys by electrochemical reduction uses liquid or solid magnesium as the cathode and carbon as the anode in a LiCl–KCl molten salt. This

technique has the advantages of simplicity, low cost, and high product purity [7, 8]. In the electrolysis process, lithium metal is generated at the cathode and reacts with magnesium to form Mg-Li alloys, while chlorine is generated at the anode. Various multicomponent Mg-Li alloys can also be produced by the addition of other metal chlorides in the molten salt [9-11]; however, the process parameters of molten salt electrolysis need to be strictly enforced to ensure suitability and stability of the reactions. Vacuum thermal reduction generally includes carbothermic [12] and silicothermic processes [13]: because of the high reduction temperature and reversible reaction of magnesium and CO gas, it is difficult to obtain pure Mg-Li alloys by vacuum carbothermic reduction. Preparation of Mg-Li alloys via vacuum silicothermic and aluminothermic reduction processes is considered as a promising approach.

Considering the demands for low energy consumption and environmental protection, a new method for producing Mg–Li alloys by vacuum aluminothemic reduction using magnesite and lithium carbonate as raw materials is proposed. The method is based on three steps: the first is calcination of magnesite and lithium carbonate, the second is



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reduction, and the third is a refining process. Figure 1 shows a flowchart of the vacuum aluminothermic reduction process.

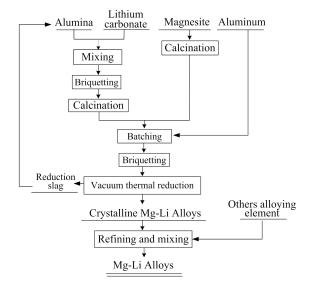


Figure 1. Flowsheet of vacuum aluminothermic reduction process

This paper presents some important data on the production of Mg–Li alloy by vacuum aluminothermic reduction using magnesite and lithium carbonate as the raw materials.

### 2. Reduction mechanisms

Magnesium and lithium metals can generally be produced by vacuum aluminothermic reduction [14, 15]. The main raw materials for producing magnesium by thermal reduction are dolomite or magnesite, while that for producing lithium is lithium carbonate.

The main component of magnesite is MgCO<sub>3</sub> and the main phase of calcined magnesite is MgO. If magnesium is produced using calcined magnesite and aluminum powder as the raw materials, the following reaction occurs:

$$4MgO(s)+2Al(l) \to 3Mg(g)+MgO \cdot Al_2O_3(s)$$
(1)  
$$\Delta G^{\theta} = 479600 - 296.81T$$

If aluminum is present in excess, MgO in the form of  $MgO•Al_2O_3$  will be reduced to metallic magnesium [16]:

$$3MgO \cdot Al_2O_3(s) + 2Al(l) \rightarrow 3Mg(g) + 4Al_2O_3(s)$$
(2)  
$$\Delta G^{\theta} = 622000 - 288.49T$$

Li<sub>2</sub>CO<sub>3</sub> is decomposed to Li<sub>2</sub>O prior to producing lithium by vacuum thermal reduction. The melting

point of  $Li_2CO_3$  is lower than its decomposition temperature, so additives are required to depress the decomposition process.  $Al_2O_3$  is the most common additive (Eq. (3)). The reduction reaction is given by Eq. (4):

$$\text{Li}_2\text{CO}_3 + \text{Al}_2\text{O}_3 \rightarrow \text{Li}_2\text{O} \cdot \text{Al}_2\text{O}_3 + \text{CO}_2 \tag{3}$$

$$\Delta G^{\theta} = 85570 - 134.39T$$

$$3\text{Li}_2\text{O} \cdot \text{Al}_2\text{O}_3 + 2\text{Al} \rightarrow 4\text{Al}_2\text{O}_3 + 6\text{Li}$$

$$\Delta G^{\theta} = 1033150 - 645.28T$$
(4)

For preparing Mg-Li alloy, the mixture of calcined magnesite (MgO) and  $\text{Li}_2\text{O}\cdot\text{Al}_2\text{O}_3$  is used as the precursor. During vacuum aluminothermic reduction, the MgO and  $\text{Li}_2\text{O}\cdot\text{Al}_2\text{O}_3$  are firstly reduced by aluminum to form Mg vapor and Li vapor in reduction furnace. The two metal vapors will form alloys in the gaseous state and then co-crystallizes on the condenser. The overall reaction is reaction (5). The content of lithium in Mg–Li alloys can be adjusted by the addition of  $\text{Li}_2\text{O}\cdot\text{Al}_2\text{O}_3$ .

$$MgO+Li_2O \cdot Al_2O_3+Al \rightarrow Al_2O_3+Mg-Li$$
 (5)

### 3. Experimental 3.1 Materials

Mg–Li alloy was produced using magnesite and lithium carbonate as the raw materials and aluminum powder as the reductant. The main components of the raw materials are listed in Table 1. Aluminum powder was produced from pure aluminum and contained > 99.5% elemental aluminum.

 Table 1. Chemical compositions of magnesite and lithium carbonate

Compounds	MgO	SiO <sub>2</sub>	$Al_2O_3$	Fe <sub>2</sub> O <sub>3</sub>	CaO	Li <sub>2</sub> CO <sub>3</sub>
Magnesite /wt.%	47.28	0.22	0.08	0.13	0.56	-
Lithium carbonate/wt.%	<0.1	< 0.01	< 0.01	< 0.01	-	>98%

#### 3.2 Experimental Method

Reduction experiments must be carried out in vacuum. The contributions of vacuum are mainly in two aspects. Firstly, the reduction temperature in vacuum could be reduced by more than 200 °C thus greatly increasing the reduction rate. Secondly, since magnesium and lithium are readily oxidizable, vacuum can prevent oxidation of both magnesium and lithium.

The reduction experiments were similar to those of the Pidgeon process. Firstly, magnesite and a mixture of lithium carbonate and alumina were separately calcined at 850 °C for 2 h. The two



calcination products were ground into powder and then mixed well with aluminum powder. The mixture was pressed into pellets and the pellets were put into a horizontal pot which was placed in reduction furnace (reduction equipment is shown in Fig. 2). Reduction was carried out at the temperature of 900-1230°C and the vacuum of 1-5 Pa. The magnesia and lithia in the pellets were reduced to metal magnesium and lithium by aluminum. Magnesium reacted with lithium to form alloys in the gaseous state and Mg-Li alloys crystallized on the condenser. The crystalline Mg-Li alloy was subsequently refined to get pure Mg-Li binary alloy. The reduction slag remained as briquettes. The reduction ratio of MgO ( $\eta$ Mg) and Li<sub>2</sub>O ( $\eta$ Li) were calculated by Eqs. (6) and (7), respectively:

$$\eta_{Mg} = (1 - \frac{\delta_{Mg} M_s}{\alpha_{Mg} M_0}) \times 100\%$$
<sup>(6)</sup>

$$\eta_{Li} = (1 - \frac{\delta_{Li}M_s}{\alpha_{Li}M_0}) \times 100\%$$
(7)

where  $M_0$  is the quantity of the raw materials and  $M_s$  is the quantity of reduction slag;  $\alpha_{Mg}$  and  $\alpha_{Li}$  are the mass percentages of MgO and Li<sub>2</sub>O in the raw materials, respectively;  $\delta_{Mg}$  and  $\delta_{Li}$  are the mass percentages of MgO and Li<sub>2</sub>O in the reduction slag, respectively.

### 4. Results and discussions

In the process of producing Mg–Li alloys by vacuum aluminothermic reduction, the content of lithium in the alloy can be adjusted by changing the relative masses of  $Li_2O$ •Al<sub>2</sub>O<sub>3</sub> and aluminum powder added. Therefore, various compositions of Mg–Li binary alloys can theoretically be produced. In this work, a Mg–Li alloy with 7% lithium content was prepared.

#### water-cooled cooling jacket water briquettes bucket $(\otimes$ $\otimes$ $\otimes$ $(\bigotimes)$ $\otimes$ cooling water reduction vacuum tube pot thermocouple cooling water resistance $\otimes$ $\otimes$ $(\otimes)$ $\otimes$ $\otimes$ furnace thermal cutoff briquettes water-cooled cooling jacket water

Mg-Li alloy condenser

### 4.1 Effect of reduction temperature on reduction ratio of MgO and Li<sub>2</sub>O

The reduction processes of MgO and  $\text{Li}_2\text{O}$  are endothermic; higher reduction temperature is advantageous for reduction reaction. Usually, the high temperature will also enhance the reaction rate. Therefore, the higher the reduction temperature is, the better the reduction proceeds. However, the reduction temperature could not exceed 1250 °C in this work because of the working temperature limit of the industrial pot used. The effects of the reduction temperature on the extents of reduction of MgO and Li<sub>2</sub>O are shown in Figure 2.

Figure 3 shows that the initial temperatures of the reductive reactions of MgO and Li<sub>2</sub>O were both lower

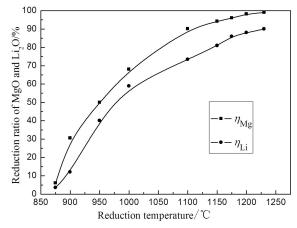


Figure 3. Effect of the reduction temperature on the reduction ratio of MgO and Li<sub>2</sub>O (excess aluminum: 3%; reduction time: 2 h)

than 900 °C. The reduction ratio of MgO and  $Li_2O$  increased with the rise of reduction temperature; however, the reduction ratio of MgO was always 10% higher than that of  $Li_2O$ , indicating that MgO was

Figure 2. Schematic drawing of the vacuum thermal reduction equipment



relatively easier to reduce by aluminum. When the reduction temperature exceeded 1200 °C, the reduction of MgO was almost complete.

### 4.2 Effect of reduction time on reduction ratio of MgO and Li,O

The time for completion of a reductive reaction depends on the reaction rate, which is mainly related to the reduction temperature, vacuum strength, and thermal conductivity of the materials. The extents of reduction of MgO and  $Li_2O$  after different reduction times are shown in Figure 4.

The extents of reduction of MgO and  $Li_2O$  increased very fast within the first 1.5 h, indicating that their reduction rates were very fast. When the

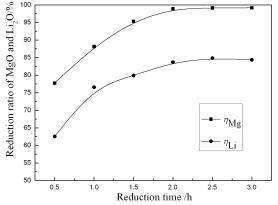


Figure 4. Effect of the reduction time on the reduction ratio of MgO and Li<sub>2</sub>O (excess aluminum: 3%; reduction temperature: 1200 °C)

reduction time exceeded 2 h, the aluminothermic reductions of MgO and  $Li_2O$  were close to completion at a reduction temperature of 1200 °C.

### 4.3 Effect of aluminum addition on reduction ratio of MgO and Li<sub>2</sub>O

As the reducing agent, the additive amount of aluminum powder has a great influence on the reduction ratio of MgO and  $\text{Li}_2\text{O}$ . In general, their reduction ratio will increase with an increase in aluminum addition, but excess addition will inevitably lower the utilization of Al. There is a balance between the cost of aluminum and the yields of lithium and magnesium. The effect of aluminum addition on the reduction ratio of MgO and  $\text{Li}_2\text{O}$  is shown in Figure 5, where zero excess aluminum refers to the stoichiometry quantity given by Eq. (5).

The reduction ratio of  $Li_2O$  increased with increasing of aluminum addition, while that of MgO was unaffected. The reduction ratio of MgO was close to 100%, so addition of excess aluminum powder was mainly used for reducing  $Li_2O$ .

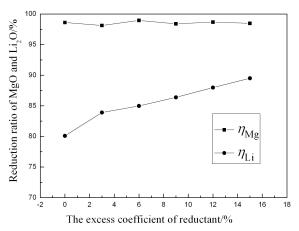


Figure 5. Effect of excess Al on the reduction ratio of MgO and Li<sub>2</sub>O (reduction time: 2 h; reduction temperature: 1200 °C)

It is generally known that most magnesium metal is produced by vacuum silicothermic reduction. Lithium metal can also be produced by vacuum thermal reduction, but the low yield (mainly because of its lower melting point) limits industrial application of this technology. Lithium that reacts with magnesium to form Mg-Li alloy in the gaseous state will raise the alloy melting point and increase the yield, but if the reductions of MgO and Li<sub>2</sub>O are not simultaneous during the reduction process, then the magnesium and lithium metals in the vapor state will crystallize separately in different areas of the crystallizer, which will decrease the yield of the alloy. The results shown in Figure 3 and 4 indicate that aluminothermic reduction of MgO and Li<sub>2</sub>O occurred simultaneously, indicating that the lithium will deport to the Mg-Li alloy and improve its yield. These conclusions were proved by the lack of reactivity of the crystalline products with water, indicating that they did not contain elemental lithium.

### 4.4 Reaction mechanisms of producing Mg-Li alloys by vacuum aluminothermic reduction

Reduction slag and crystalline Mg–Li alloys were obtained after the reduction process; pure Mg–Li alloys can hence be obtained by remelting and refining the crystalline Mg–Li alloys. However, it is necessary to emphasize that the crystalline Mg–Li alloys produced by vacuum thermal reduction contain impurities, mainly oxide impurities and metal impurities; SiO<sub>2</sub>, Al<sub>2</sub>O<sub>3</sub>, Fe<sub>2</sub>O<sub>3</sub>, CaO, and Na<sub>2</sub>O are the main impurities of raw materials. In reduction process, Fe<sub>2</sub>O<sub>3</sub>, CaO, and Na<sub>2</sub>O can be reduced and some Na and Ca may be crystallized with Mg-Li alloy. The refining agent are mainly KCl, MgCl<sub>2</sub>, LiCl, and LiF. In refining process, the oxide impurities, Ca and Na, will react with MgCl<sub>3</sub> and LiCl



to produce CaCl<sub>2</sub> and NaCl. The other impurities are very few. The refined Mg–Li alloys can fully meet the standard. An X-ray diffraction (XRD) analysis of the crystalline Mg–Li alloy is presented in Figure 6.

As shown in Figure 4, the extent of reduction of MgO was always higher than that of  $Li_2O$ , which relates to the reaction mechanism of their aluminothermic reductions. XRD patterns of the reduction slag at temperatures between 900 °C and 1200 °C are displayed in Figure 7.

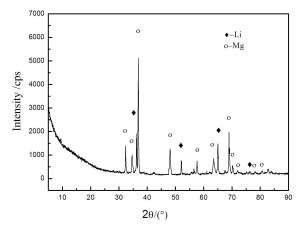


Figure 6. X-ray diffraction analysis of crystalline Mg–Li alloy

According to the XRD analysis of the reduction slag, MgO and  $Li_2O \cdot Al_2O_3(LiAIO_2)$  were first reduced to Mg and Li by aluminum at a low temperature to form MgO \cdot Al\_2O\_3 (as shown in Eqs. (1) and (8)). Li\_2O in form of Li\_2O \cdot Al\_2O\_3 and MgO in form of MgO \cdot Al\_2O\_3 (as shown in Eqs. (9) and (10)). Li\_2O \cdot 5Al\_2O\_3 (as shown in Eqs. (9) and (10)). Li\_2O \cdot 5Al\_2O\_3 is more stable than MgO \cdot Al\_2O\_3, so the reduction of MgO in the form MgO \cdot Al\_2O\_3 was

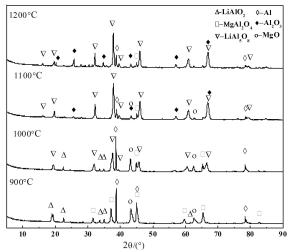


Figure 7. X-ray diffraction analysis of reduction slag (reduction time: 2 h; excess aluminum: 3%; reduction temperature: 1200 °C)

relatively easier than that of  $Li_2O$  in the form of  $Li_2O\bullet 5Al_2O_3$ .  $Li_2O$  in the form of  $Li_2O\bullet 5Al_2O_3$  can be reduced further (Eq. (11)), but this requires additional aluminum, which would significantly reduce its utilization ratio and therefore undoubtedly increase the cost of the reduction process.

$$MgO+4(Li_2O \cdot Al_2O_3)+2Al \rightarrow 4MgO \cdot Al_2O_3+Mg+8Li \qquad (8)$$

$$4(\text{Li}_2\text{O} \cdot \text{Al}_2\text{O}_3) + 2\text{Al} \rightarrow \text{Li}_2\text{O} \cdot 5\text{Al}_2\text{O}_3 + 6\text{Li}$$
(9)

$$3MgO \cdot Al_2O_3 + 2(Li_2O \cdot Al_2O_3) + 3Al \rightarrow$$
(10)

Li<sub>2</sub>O·5Al<sub>2</sub>O<sub>2</sub>+3Mg+3Li

$$3(\text{Li}_2\text{O} \cdot 5\text{Al}_2\text{O}_3) + 2\text{Al} \to 16\text{Al}_2\text{O}_3 + 6\text{Li}$$
 (11)

## 4.5 Effect of $Li_2O \cdot Al_2O_3$ addition in raw materials on reduction process

Theoretically, a wide range of Mg–Li binary alloys can be produced by adjusting the proportion of  $Li_2O \cdot Al_2O_3$  added to the raw material mixture. However, the lithium content of Mg–Li binary alloys cannot be too high because a higher lithium content correlates with a lower melting point of the alloy, which would decrease its yield. According to the Mg– Li binary alloy phase diagram, the lithium content should not exceed 40% to avoid affecting the yield. The effect of  $Li_2O \cdot Al_2O_3$  addition (i.e., the content of lithium in Mg–Li alloys) on the extents of reduction of MgO and  $Li_2O$  is shown in Figure 8; the XRD patterns of the respective slags are shown in Figure 9.

As shown in Figures 8 and 9, the main phases of the reduction slags were similar, but the reduction ratio of Li<sub>2</sub>O increased when the Li<sub>2</sub>O•Al<sub>2</sub>O<sub>3</sub> addition increased. The highest extent of reduction exceeded 96%. Increasing the proportion of Li<sub>2</sub>O•Al<sub>2</sub>O<sub>3</sub> added decreased the relative proportion of MgO, and hence the amount of alumina produced from the reduction of MgO by aluminum, which further reduced the amount

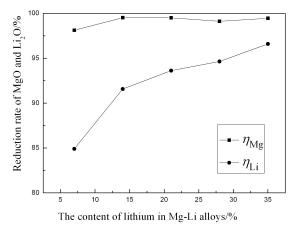


Figure 8. Effect of Li<sub>2</sub>O•Al<sub>2</sub>O<sub>2</sub> addition on the reduction ratio of MgO and Li<sub>2</sub>O (reduction time: 2 h; excess aluminum: 3%; reduction temperature: 1200 °C).



of  $Li_2O$  in the form of  $Li_2O$ •5 $Al_2O_3$ . This is the primary reason for the increase in the extent of reduction. Another reason is the increase in contact area between  $Li_2O$  and aluminum.

The reduction slag contains mainly  $Li_2O$  (about 0.5%–0.8%) and  $Al_2O_3$ , so it can be reused as an additive to the calcination process, as shown by the reduction reaction given as Eq. (12):

$$Li_2O \cdot 5Al_2O_3 + 4Li_2CO_3 \rightarrow 5(Li_2O \cdot Al_2O_3) + 4CO_2$$
(12)

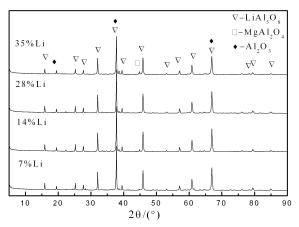


Figure 9. X-ray diffraction analysis of reduction slags produced by varying Li<sub>2</sub>O•Al<sub>2</sub>O<sub>3</sub> addition to the raw material

### 5. Conclusions

(1) A method of producing Mg–Li alloys by vacuum aluminothermic reduction using magnesite and lithium carbonate as the raw materials was proposed. In the reduction process, the extent of reduction of MgO was always higher than that of Li<sub>2</sub>O, indicating that MgO was relatively easier to reduce by aluminum. The reduction ratio of MgO was almost 100% and that of Li<sub>2</sub>O exceeded 96%. The main phase of the reduction slag was Li<sub>2</sub>O•5Al<sub>2</sub>O<sub>3</sub>. Li<sub>2</sub>O in the form of Li<sub>2</sub>O•5Al<sub>2</sub>O<sub>3</sub> is difficult to reduce, which is the main reason for the lower reduction ratio of Li<sub>2</sub>O.

 $(\bar{2})$  Compared with other vacuum thermal reduction process, the aluminothermic reduction process can achieve simultaneous reduction of MgO and Li<sub>2</sub>O and zero discharge of waste residues. Therefore, it can be regarded as a highly efficient and environmental friendly method with low energy consumption and low emissions of waste residues.

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# PROIZVODNJA Mg-Li LEGURA ALUMINOTERMIČKOM REDUKCIJOM U VAKUUMU

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### Apstrakt

Mg-Li legure predstavljaju najlakše metalne građevinske materijale i jedne od najreprezentativnijih legura lakih metala. U ovom radu je ispitivan postupak dobijanja legure magnezijuma i litijuma putem aluminotermičke redukcije u vakuumu, prilikom koga se kao sirovine koriste magnezit i litujum karbonat. Uticaj parametara redukcije na opseg redukcije MgO i  $Li_2O$  je takođe ispitivan. Rezultati su pokazali da se Mg-Li legure mogu dobiti postupkom aluminotermičke redukcije u vakuumu kada se koriste kalcinisani magnezit i litijum karbonat. Donekle je lakše redukovati MgO od  $Li_2O$  u prisustvu aluminijuma. Skoro se sav MgO redukovao u Mg, a više od 96%  $Li_2O$  je redukovano u Li. Glavna faza u šljaci dobijenoj redukcijom je  $Li_2O$ -SAl $_2O_3$ . Razmatrani su i mehanizmi reakcije. Aluminotermička redukcija u vakuumu se može smatrati veoma efikasnom i ekološkom metodom za dobijanje Mg-Li legura.

Ključne reči: Mg-Li legura; Aluminotermička redukcija u vakuumu; Magnezit; Litijum karbonat; Li<sub>2</sub>O•5Al<sub>2</sub>O<sub>3</sub>

