

TRANSIENT HEAT TRANSFER AND SOLIDIFICATION MODELING IN DIRECT-CHILL CASTING USING A GENERALIZED FINITE DIFFERENCES METHOD

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Abstract

The goal of this work is to achieve a novel solution of the transient heat transfer problem in the start-up phase of direct-chill casting processes using a Generalized Finite Differences Method. This formulation is applied in order to solve the heat transfer equation in strong form under a Lagrangian description. The boundary conditions incorporation is done in a simple and natural way. The meshfree nature of this approach allows to capture the motion and phase boundaries evolution without using remeshing approaches. The simplicity, efficiency and suitability of this numerical formulation is demonstrated by comparison of the obtained numerical results with the results already published by other researchers. This shows that our approach is promising for the numerical simulation of heat transfer problems during the start-up phase of direct-chill casting processes.

Keywords: *Finite Pointset Method; Heat transfer; Direct-chill casting; Start-up phase; Solidification*

1. Introduction

Semi-continuous casting techniques are the most used processes for mass-production of aluminum alloys. One of these techniques is the so-called "Direct-Chill Casting" method (DCC) [1]. It begins with a step in which molten metal is poured into a water-cooled mould where heat from the nearby mould walls is extracted causing its solidification. Once the metal leaves the mould cooling zone, it is further cooled in a secondary cooling zone where water is sprayed on the casting surface. This cooling process continues until the casting reaches the possible maximum length [2]. One of the most important phases in the DCC process is the start-up phase which is the period from the operation start to the time when a steady state is achieved. This phase is highly important since many defects in the end product could originate during this step. In order to get homogeneous casting products, the control of process parameters as cooling rates, casting speed, inlet velocities, and the casting temperature is needed. Notwithstanding, it is hard to optimize and enhance these techniques with experimental studies because it is very tough to quantify temperatures, stresses fields, pressures, or velocities, especially within the mould

region during the start-up phase where complex physical phenomena exist [3]. Numerical modelling and simulation is commonly used to improve and prevent the occurrence of casting defects because it produces a lot of detailed information which cannot be obtained with other kind of techniques [4].

The numerical modelling and simulation of physical phenomena involved in continuous casting (CC) and DCC processes are usually based on classical mesh – based approaches [5]. For example, several numerical algorithms based on Finite Element Method (FEM) have been developed for the modelling of three-dimensional fluid flow, heat transfer, and solidification in CC processes [6], the analysis of convective heat transfer in the molten metal and phase change in aluminum DCC [7], prediction of stresses, strains, mushy zone length, and heat transfer in DCC [8], the study of cooling and solidification of semi-continuous casting processes of copper [9], determination of two-fluid flow and the meniscus interface movement in an electromagnetic CC of steel [10], heat transfer study in the primary cooling zone in DCC using experimental measurements of the ingot, mould, and cooling water temperatures during casting [11], the simulation of mould cavity filling process, study of the influence of

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molten steel flow, and the pouring types on the solidification kinetics at the initial stage in CC [12].

Other numerical approaches based on the Finite differences Method (FDM) have been used to model the steady-state three-dimensional heat flow in CC of steel [13], the numerical prediction of 3D laminar or turbulent liquid flow, heat transfer, and macroscopic solidification in DCC of aluminum alloys to investigate the temperature distributions and solidification patterns in the mould and post mould regions [14], and the analysis of the steady-state heat transfer phenomena in CC [15]. Similarly, numerical procedures based on the Finite Volume Method (FVM) have been proposed for the prediction of turbulent flow and temperature in complex flows of molten steel in CC [16], and the modeling of heat transfer and solidification in CC, considering the establishment of experimental non-uniform and uniform water distributions for the cooling conditions [17].

Meshless or meshfree methods have been developed in recent decades as an alternative to the classical mesh-based techniques since they allow to overcome some of the drawbacks in such methods [18]. The advantages of meshfree methods over mesh-based methods rely on the fact that they use a set of finite nodes scattered within a domain of interest as well as on its boundaries, without needing some information with respect to the connectivity and relations between particles such that they do not constitute a mesh of elements. This makes them very attractive in problems involving high deformations and discontinuities in the computational domain without employing remeshing techniques. As a result, it gives the freedom to remove or incorporate particles whenever and wherever required, allowing a simple development of adaptive strategies.

The Local Radial Basis Function Collocation Method (LRBFCM) is a strong form meshless method that has been used for the numerical simulation of CC process of steel considering turbulent fluid flow and solidification [2], the simulation of transient heat transfer of the start-up phase in DCC of aluminum alloys [19], and the simulation of DCC under the influence of a low-frequency electromagnetic fields [20]. Other strong form meshless method approach that has been tested for the modeling of heat transfer and solidification in CC processes in the primary and secondary cooling regions is the Oñate's Finite Point Method (FPM) [21].

Apart from the mentioned meshless methods given in strong form, there exist some other weak form approaches such as the element-free Galerkin method (EFG) that has been used for the simulation of transient heat transfer of the start-up phase in DCC of an aluminum alloy round billet considering the non-linear aspects related to the material properties and

boundary conditions [22]. Recently, another weak form meshless method that has been tested in the analysis of the solidified shell thickness, the mushy zone thickness, the metallurgical length, and residual stress in CC processes is a 3D thermo-elastoplastic Petrov–Galerkin (MLPG) method [23].

A truly meshfree Generalized Finite difference Method (GFDM) is the Finite Pointset Method (FPM) proposed by J. Kuhnert [24]. It has shown to be much better than other meshfree methods and the long-established mesh-based methods for treating multiphase or free surface flows, fluid mechanics problems involving quickly evolving domains, and for problems including heat transfer or convective flows [25, 26, 27]. It is a Lagrangian method of strong-form that utilizes a weighted least-squares (WLSM) method to solve elliptic partial differential equations and to compute spatial derivatives [28]. It has numerous advantages when compared with other numerical techniques because it is capable of simply and naturally incorporating any form of boundary condition without requiring some stabilization or special treatments, and its implementation is straightforward [27]. Nevertheless, the transient problem arising in semi-continuous casting processes has not been tested yet. Consequently, the application of FPM to analyze the transient heat transfer and solidification problems in direct-chill casting is proposed in this work; to the author's knowledge this is the first time that this approach has been applied in order to solve this practical engineering industrial process in metal casting. With the purpose of getting some information on its performance, the numerical solution of the start-up phase in a DCC example is compared with numerical published data predicted by other researchers using different numerical methods. The structure of this article is as follows: Section 2 describes the partial differential equation to be considered. Section 3 describes the ideas behind FPM and the numerical scheme applied for the solution of the governing equations. The numerical examples and their results are presented in Section 4. Finally, in the last section some conclusions are given.

2. Governing Equations

The modeling of the transient heat transfer and solidification in DCC will be done by means of the heat transfer equation which in Lagrangian form is given by

$$\rho c \frac{DT}{Dt} = \nabla \cdot (k \nabla T) \quad (1)$$

where c is the specific heat, k is the conductivity, T is the temperature, ρ is the density and t is the time. The problem is defined with proper initial and



boundary conditions.

The initial and boundary conditions for this problem are

$$T|_{\partial\Omega_i, t=0} = T_0 \tag{2}$$

$$k\nabla T \cdot \mathbf{n}|_{\partial\Omega_q} = q|_{\partial\Omega_q} \tag{3}$$

where $\partial\Omega$ indicates the kind of boundary, $\partial\Omega_k$ denotes an inflow boundary condition and $\partial\Omega_1$ refers to a wall boundary condition, q is the heat flux density, \mathbf{n} is the outward unitary normal vector on $\partial\Omega$ and T_0 is the initial temperature. Furthermore, $q=0$ for isolated boundaries or $q=h_c(T-T_\infty)$ in convective boundaries, where T_∞ is a reference temperature and h_c is the convective heat transfer coefficient.

3. Numerical Scheme

In this section we present the ideas behind FPM, and the numerical scheme applied for the solution of this transient heat transfer problem in DCC. We start with a temporal discretization of Eq. (1) using an implicit Euler scheme, which leads to

$$\rho c T^{(n+1)} - \Delta t \nabla \cdot (k \nabla T^{(n+1)}) = \rho c T^n \tag{4}$$

where the superscripts indicate the level of time for T and Δt is the time step. Eq. (4) can be rewritten in general form as

$$AT^{(n+1)} + B(\nabla T^{(n+1)}) + C\nabla^2 T^{(n+1)} = D \tag{5}$$

where A , B , C and D are defined as: $A=\rho c$, $B=\Delta t \nabla k$, $C=k \Delta t$ and $D=\rho c T^n$ [26].

3.1 The Finite Pointset Method

In this subsection, the general ideas behind FPM are described, which is a GFDM that uses the WLSM. Following [27, 28]:

Let Ω be a material domain with boundary $\partial\Omega$ and suppose that a set of nodes $\mathbf{r}_1, \mathbf{r}_2, \dots, \mathbf{r}_N$ are distributed with corresponding function values $f(\mathbf{r}_1), f(\mathbf{r}_2), \dots, f(\mathbf{r}_N)$. Then, we are interested in computing the value of f at whatever location $f(\mathbf{r})$ using the function values at node positions in the vicinity of \mathbf{r} . A weight function $w(\mathbf{r}_i - \mathbf{r})$ is proposed in order to determine the number of nodes and the vicinity of \mathbf{r} whose form is

$$w_i = w(\mathbf{r}_i - \mathbf{r}; h) = \begin{cases} e^{-\alpha \frac{\|\mathbf{r}_i - \mathbf{r}\|^2}{h^2}}, & \|\mathbf{r}_i - \mathbf{r}\| \leq h \\ 0, & \text{differently} \end{cases} \tag{6}$$

where \mathbf{r}_i is the position of the i -th node in the vicinity of \mathbf{r} , α is a positive constant with a value of 6.5 and h is the smoothing length. A Taylor's series

approximation of $f(\mathbf{r}_i)$ around \mathbf{r} is

$$f(r_i) = f(r) + \sum_{k=1}^3 f_k(r)(r_{ki} - r_k) + \frac{1}{2} \sum_{k,l=1}^3 f_{kl}(r)(r_{ki} - r_k)(r_{li} - r_l) + e_i \tag{7}$$

where f_k and f_{kl} ($f_{kl} = f_{lk}$) depict the set of first and second spatial derivatives at the node position \mathbf{r} , r_{ki} and r_k are the k -th components of the positions \mathbf{r}_i and \mathbf{r} , respectively, and e_i is the truncation error. f_k and f_{kl} can be determined minimizing e_i for the n_p Taylor's series approximations of $f(\mathbf{r}_i)$ for to the n_p nodes in the \mathbf{r} vicinity. The resultant system of equations can be expressed in matrix form as

$$e = Ma - b \tag{8}$$

with

$$e = [e_1, e_2, \dots, e_{n_p}]^t \tag{9}$$

$$a = [f, f_1, f_2, f_3, f_{11}, f_{12}, f_{13}, f_{22}, f_{23}, f_{33}]^t \tag{10}$$

$$b = [f(r_1), f(r_2), \dots, f(r_{(n_p)})]^t \tag{11}$$

$$M = [s_1, s_2, \dots, s_{n_p}]^t \tag{12}$$

$$s_i = [1, \Delta r_{1i}, \Delta r_{2i}, \Delta r_{3i}, \Delta r_{11i}, \Delta r_{12i}, \Delta r_{13i}, \Delta r_{22i}, \Delta r_{23i}, \Delta r_{33i}] \tag{13}$$

with $\Delta r_{ki} = r_{ki} - r_k$, $\Delta r_{kli} = (r_{ki} - r_k)(r_{li} - r_l)$ and $\Delta r_{kkli} = 0.5(r_{ki} - r_k)^2$, where $k \neq l$ and $k, l = 1, 2, 3$.

The value of \mathbf{a} is computed with WLSM minimizing the quadratic form

$$J = \sum_{i=1}^n w_i e_i^2 \tag{14}$$

which reads $(M^t W M) \mathbf{a} = (M^t W) \mathbf{b}$, where $W = \text{diag}(w_1, w_2, \dots, w_{n_p})$. Therefore, $\mathbf{a} = (M^t W M)^{-1} (M^t W) \mathbf{b}$. Thereby, the values of the function and its derivatives at \mathbf{r} are automatically calculated.

3.2 FPM form for general elliptic partial differential equations

General elliptic partial differential equations like Eq. (5) have been studied earlier in [25]. Thus, in this subsection we present the corresponding FPM discretization for these general equations [27]. For solving a general elliptic equation with FPM, Eq. (5) must be taken along with the system of n_p Taylor's series approximations of $f(\mathbf{r}_i)$ around \mathbf{r} . On this occasion, the matrices involved in the computation have the following new form: $\mathbf{b} = [f(\mathbf{r}_1), f(\mathbf{r}_2), \dots, f(\mathbf{r}_{n_p}), D]^t$, $M = [s_1, s_2, \dots, s_{n_p}, s_E]^t$, and $W = \text{diag}(w_1, w_2, \dots, w_{n_p}, I)$,



where $s_E = [A, B_1, B_2, B_3, C, 0, 0, C, 0, C]^T$ and $\mathbf{B} = [B_1, B_2, B_3]^T$.

If $r \in \partial\Omega$, we have to incorporate the corresponding boundary conditions in the system of equations. For the special case of this transient heat transfer problem in DCC, the boundary conditions (3) have the general form

$$ET + n \cdot \nabla T = F \quad (15)$$

Thus, for this boundary condition the matrices involved in the computation are:

$$b = [f(r_1), f(r_2), \dots, f(r_{n_p}), D, F]^T \quad (16)$$

$$M = [s_1, s_2, \dots, s_{n_p}, s_E, s_B]^T \quad (17)$$

and

$$W = \text{diag}(w_1, w_2, \dots, w_{n_p}, 1, 1) \quad (18)$$

where $s_B = [E, n_1, n_2, n_3, 0, 0, 0, 0, 0, 0]$.

If we define $\mathbf{Q} = [Q_1, Q_2, \dots, Q_{10}]$ being the first row of $(MWM)^{-1}$, and the terms in the WLSM solution $\mathbf{a} = (MWM)^{-1}(MW)\mathbf{b}$ are explicitly calculated, we can notice that the next linear equations result

$$\sum_i^{n(j)} w_i (Q_1 + Q_2 \Delta r_{1i} + Q_3 \Delta r_{2i} + Q_4 \Delta r_{3i} + Q_5 \Delta r_{11i} + Q_6 \Delta r_{12i} + Q_7 \Delta r_{13i} + Q_8 \Delta r_{22i} + Q_9 \Delta r_{23i} + Q_{10} \Delta r_{33i}) f(r_i) = [AQ_1 + B_1 Q_2 + B_2 Q_3 + B_3 Q_4 + (Q_5 + Q_8 + Q_{10})C]D + [EQ_1 + n_1 Q_2 + n_2 Q_3 + n_3 Q_4]F \quad (19)$$

where $f(r_j)$ represents the unknown function value at the node j and $n(j)$ the number of j -th nodes in the vicinity. As Eq. (19) holds for $j = 1, 2, \dots, N$, it forms a full sparse system of linear equations $LT = \mathbf{P}$ that can be solved with iterative procedures. Therefore, any kind of solidification and thermal phenomena governed by Eq. (1,5) can be computed with this procedure, just aggregating proper entries in the systems of equations [25, 26].

4. Numerical Examples and Results

With the goal of validating the suitability of this FPM approach to model the transient heat transfer problem in the start-up phase of the DCC process, the solution of a heat transfer and solidification general benchmark problem and the solution of a simplified model of the start of the DCC process in axisymmetry are reported and compared with the published numerical and theoretical data [19, 22].

4.1 Solidification in an infinite corner

This transient heat transfer and solidification general benchmark problem corresponds to an infinite corner of liquid that starts to freeze under a Dirichlet boundary temperature condition. This example was

selected since it allows to validate the proposed FPM formulation against the results of an analytically solvable two-dimensional solidification problem [29]. In this example, an infinite corner of liquid with a uniform initial temperature $T_0 = 273.45$ K starts to freeze under a Dirichlet boundary temperature condition $T_D = 272.15$ K on the lower left corner, and in the rest of the edges a Neumann outflow boundary condition was used without taking into account the convective fluid flow generated during the cooling. The melting temperature of the liquid in the corner is $T_m = 273.15$ °C, whilst its thermal properties at the melting point are: $c_m = 1$ J/kg K, $k_m = 1$ W/mK and $\rho_m = 1$ kg/m³. In this example the thermal conductivity and the specific heat of the solid and liquid phases are assumed to be equal to their corresponding values in the melting point.

The effect of the latent heat is included through an effective heat capacity. The latent heat of this fluid is taken as $h_f = 0.25$ J/kg and the computation was performed for 0.5 s. The numerical solution was obtained considering a squared geometry of 3 m of length with two point clouds (PC) with 2601 and 441 points with a mean spacing of 0.06 m and 0.15 m, respectively. The smoothing length used in the fine PC simulation was chosen as 0.192 m and the time step was selected as $\Delta t = 0.001$ s. Finally, the smoothing length used in the coarse PC simulation was chosen as 0.48 m and the time step was selected as $\Delta t = 0.005$ s.

The analytical solution for the solidification front location assuming constant thermal properties and densities is given by Stapor [29] and it reads

$$y = \left(0.17625 + \frac{0.159}{\left(\frac{x}{\sqrt{4\alpha t}}\right)^{5.02} - 0.17625} \right) \sqrt{4\alpha t} - 1.5 \quad (20)$$

where $\alpha = k / \rho c = 1 \text{ m}^2/\text{s}$

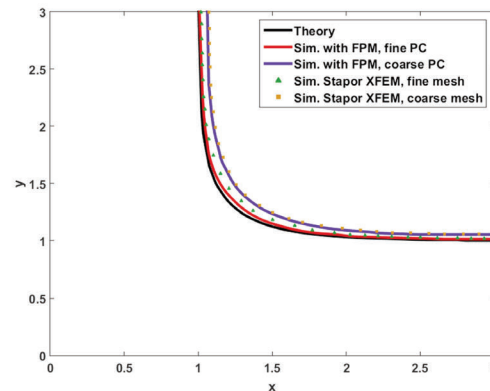


Figure 1. Solidification front at $t = 0.5$ s, where x and y axis denote the distance from the lower left corner where the Dirichlet boundary condition is imposed



The solidification front location at $t = 0.5$ s obtained by means of this FPM formulation is shown and compared with the previous analytical solution, and with the XFEM simulation results of Stapor [29] in Figure 1. In this case the interphase position calculated with FPM perfectly matches the analytical solution and the Stapor's XFEM simulation with a fine mesh. Further, it could be observed that the solidification front position predicted by FPM with a coarser point cloud is closer to the analytical solution than the corresponding numerical solution obtained with XFEM. These results show that this FPM formulation works very well for the computation of heat transfer and solidification processes.

4.2 Simplified model of the start-up phase in a DCC process

Once the FPM formulation was tested for the previous example of heat transfer and solidification, the next natural step is to model and obtain a numerical approximation of the thermal effects involved in the start-up phase of a DCC process. With this purpose in mind, the simplified model of the start of the DCC process in axisymmetry studied by Vertnik et al. in [19] was selected.

The initial configuration of this problem is a cylinder, $0 \leq z \leq 0.01$ m, $0 \leq r \leq 0.25$ m, whose initial temperature is T_0 . The boundary conditions on $z=0$ are of Dirichlet type with $T(z=0)=T_0$, and the boundaries at the moving bottom are isolated. The boundary conditions at the outer surface are of the Robin type with a reference temperature T_∞ .

Table 1. Convective heat transfer coefficients h_c along the casting direction

Axial position / m	Convective heat transfer coefficient / W/m ² K
$0 \leq z \leq 0.01$	0
$0.01 \leq z \leq 0.06$	3000
$0.06 \leq z \leq 0.1$	150
$0.1 \leq z \leq 1.25$	4000

Table 2. Process parameters used for the numerical simulation

Parameter	Value
Initial temperature, T_0	980 K
Reference temperature, T_∞	298 K
Liquidus Temperature, T_L	911 K
Solidus Temperature, T_S	775 K
Liquid thermal conductivity, k_L	57.3 W/mK
Solid thermal conductivity, k_S	120.7 W/mK
Liquid density = Solid density, $\rho_L = \rho_S$	2982 kg/m ³
Liquid specific heat, c_L	1179 J/kgK
Solid specific heat, c_S	1032 J/kgK
Fusion latent heat, h_f	348.2 kJ/kg
Casting speed, v_z	0.000633 m/s

In this study case the convective heat transfer coefficients are distributed as shown in Table 1 and the material properties are specified in Table 2. In this formulation, the effect of the latent heat was taken into account using the effective heat capacity method: $c = c_s f_s + c_L (1 - f_s) + h_f (\partial f_s / \partial T)$. The liquid fraction increases linearly with temperature between T_L and T_S . The thermal conductivity in the mushy zone vary linearly with temperature as $k_m = k_s f_s + k_L (1 - f_s)$, where f_s is the solid fraction and it is defined as

$$f_s(T) = \begin{cases} 1, & T \leq T_S \\ \frac{T_L - T}{T_L - T_S} & T_S < T \leq T_L \\ 0, & T \geq T_L \end{cases} \quad (21)$$

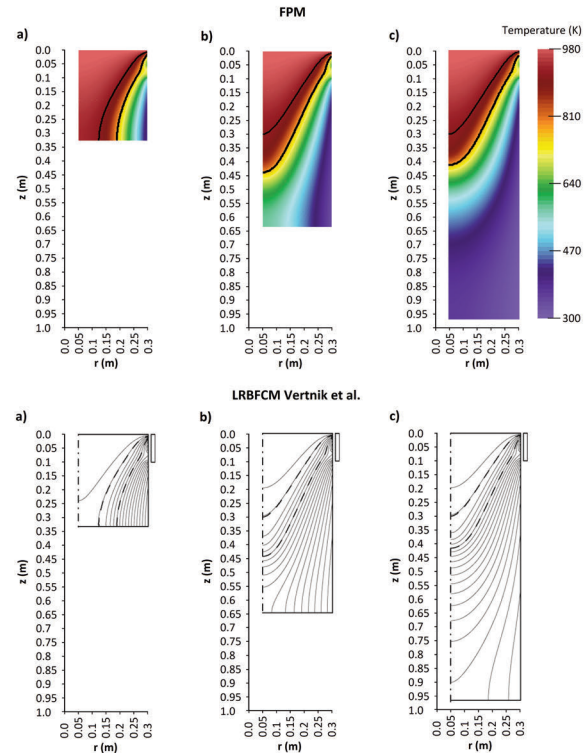


Figure 2. Temperature profiles and the liquidus and solidus isotherms at a) 500 s, b) 1000 s and c) 1500 s predicted by FPM (top) and LRBFCM Vertnik et al. [19] solution (bottom)

The smoothing length used in this simulation was $h = 0.00875$ m with a time step $\Delta t = 0.1$ s. The solution of this example has been obtained with an initial discretized domain of 505 nodes with an average spacing of 0.0025 m. In this example, the domain growth is imposed moving the current point cloud according with the casting speed, and adding a new row of nodes in $z=0$ when a gap with the size of the initial mean spacing is formed.



The temperature profiles over the billet at different time steps predicted by this formulation of FPM are shown in Figure 2 where a comparison with the corresponding numerical results of Vertnik et al. [19] is shown. As it can be seen in this picture, the temperature distributions, and the liquidus and solidus isotherms predicted by FPM match very well with their numerical counterparts in [19].

Further, these figures depict smooth and physical temperature fields with a stable evolution through time. This indicates the FPM potential for the numerical simulation of this start-up DCC transient heat transfer problem since the accuracy of the solutions is appropriate, and the non-linear aspects related to material domain growth and the phase changes are well reproduced.

In Figure 3, the centerline, mid-radius, and surface temperatures at different time steps predicted by this formulation of FPM together with the corresponding numerical results of Vertnik et al. [19] are shown. Regarding the computed temperature along these lines, the graphs are in a very good agreement. However, minor differences in the temperatures up to

around 7 K can be observed in some points which are directly attributed to the differences in the numerical approaches. Further, in the FPM solution the domain growth was imposed moving the whole current point cloud according with the casting speed, whilst in [19] the domain growth was imposed moving only the boundary points at the end of the billet according with the casting speed, and adding a new row of points between the boundary and inner ones when it is needed. Nevertheless, these results show the effectiveness of this approach to model the transient thermal behavior and the evolution of the solidified shell thickness in the start-up phase in DCC.

5. Conclusions

Once the current formulation of FPM was implemented and tested in a simplified model of the start-up phase in a DCC process, the following could be concluded:

1. This approach could be used properly to simulate this kind of transient heat transfer and solidification problems in DCC.

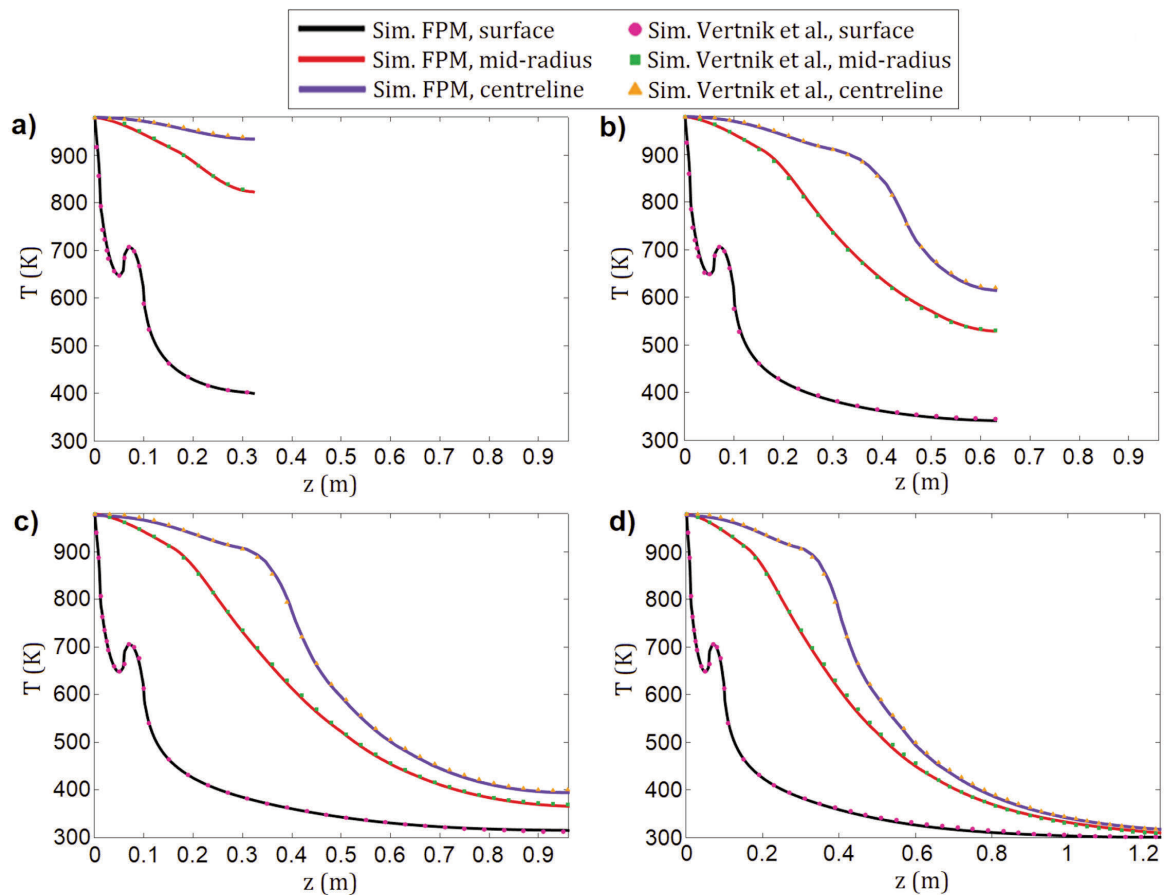


Figure 3. Comparison of centerline, mid-radius, and surface temperatures predicted by FPM with the corresponding LRBFCM Vertnik et al. [19] solution at: a) 500 s, b) 1000 s, c) 1500 s and d) steady-state solution (2100 s)

2. This approach has shown an excellent behavior for the numerical simulation of these transient problems.

3. This is the first time, to the author's knowledge, that the discussed version of FPM for transient heat transfer and solidification in DCC has been successfully tested for this industrial process.

4. The range of application of FPM has been extended in this work in the context of DCC.

5. Since this formulation is a truly meshless method, there is no need to keep a regular node distribution in order to obtain good numerical

approximating solutions, not even to compute any numerical quadrature.

6. It can be used in the future for the analysis of more complex problems in the start-up phase in DCC as the coupling of transient heat transfer and fluid flow.

7. FPM is promising since it is a feasible and a much simpler approach for implementation; it is able to handle high deformations in the domain, and finally, it is capable of naturally incorporating any form of boundary condition without requiring some stabilization or special treatments.

Nomenclature

A	PDE coefficient / 1	k	Thermal conductivity / W/m K
B	PDE coefficient / 1	k_m	Thermal conductivity at melting point / W/m K
C	PDE coefficient / 1	k_L	Liquid thermal conductivity / W/m K
D	PDE coefficient / 1	k_s	Solid thermal conductivity / W/m K
E	PDE coefficient / 1	\mathbf{n}	Boundary normal vector / 1
F	PDE coefficient / 1	n_p	Number of neighbor points / 1
J	Functional / 1	q	Local heat flux density / W/m ²
M	Differences matrix / 1	\mathbf{r}	Particle position / m
\mathbf{Q}	Auxiliary vector / 1	\mathbf{r}_i	i -th particle position / m
T	Temperature / K	r_k	k -th components of \mathbf{r} / m
T_0	Initial temperature / K	r_{ki}	k -th components of \mathbf{r}_i / m
T_∞	Reference/ambient temperature / K	\mathbf{s}_i	i -th Differences vector / 1
T^n	Temperature at n -th time step / K	t	Time / s
T_D	Dirichlet temperature / K	v_z	Casting speed / m/s
T_m	Melting temperature / K	w	Weight function / 1
T_L	Liquidus temperature / K	y	Vertical coordinate / m
T_s	Solidus temperature / K	z	Axial coordinate / m
W	Weight matrix / 1	α	Weight function parameter / 1
\mathbf{a}	Unknowns vector / 1	α'	Auxiliary variable / m ² /s
\mathbf{b}	Unknowns vector / 1	ρ	Density / kg/m ³
c	Effective specific heat / J/kg K	ρ_m	Density at melting point / kg/m ³
c_m	Specific heat at melting point / J/kg K	ρ_L	Liquid density / kg/m ³
c_L	Liquid Specific heat / J/kg K	ρ_s	Solid density/ kg/m ³
c_s	Solid Specific heat / J/kg K	Δr_{ki}	First order spatial differences / m
\mathbf{e}	Truncation error vector / 1	Δr_{lki}	Second order spatial differences / m ²
f	Arbitrary function value / 1	Δt	Time step size / s
f_k	First spatial derivative / 1	∇	Gradient operator / m ⁻¹
f_{kl}	First spatial derivative / 1	D/Dt	Material derivative / s ⁻¹
f_s	Solid fraction / 1	Ω	A given domain / 1
h	Smoothing length / m	$\partial\Omega$	Boundary of the domain / 1
h_c	Convective heat transfer coefficient / W/m ² K	$\partial\Omega_k$	Inflow boundary / 1
h_f	Fusion latent heat / J/kg	$\partial\Omega_l$	Wall boundary / 1



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MODELIRANJE PRELAZNOG PRENOSA TOPLOTE I SOLIDIFIKACIJE TOKOM DIREKTNOG HLADNOG LIVENJA KORIŠĆENJEM OPŠTE METODE KONAČNIH RAZLIKA

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Apstrakt

Cilj ovog rada je da pronađe novo rešenje za problem prelaznog prenosa toplote u početnoj fazi procesa direktnog hladnog livenja korišćenjem opšte metode konačnih razlika. Ova formulacija je primenjena da bi se rešila jednačina prenosa toplote po proširenom modelu Lagranžove jednačine. Uključivanje graničnih uslova urađeno je na jednostavan i prirodan način. Bezmrežna priroda ovog pristupa omogućava da se dobije kretanje i evolucija graničnih faza bez korišćenja metoda ponovnog umrežavanja. Jednostavnost, efikasnost i primerenost ove numeričke formulacije dokazuje se poređenjem dobijenih numeričkih rezultata sa rezultatima koje su drugi istraživači već objavili. Ovo pokazuje da je naš pristup obećavajući što se tiče numeričke simulacije problema prenosa toplote tokom početne faze procesa direktnog hladnog livenja.

Ključne reči: Metod konačnih elemenata; Prenos toplote; Direktno hladno livenje; Početna faza; Solidifikacija

